

EngrD 2190 – Lecture 11

Concept: Process Analysis – Mathematical Modeling with Energy Balances

- One cannot measure energy; one must use measurable quantities (temperature and phase) and convert to energy.
- One cannot calculate absolute energy; one must calculate energy *change*.

Context: A heater, a heater + partial evaporator, and a heat exchanger.

Defining Question: What is an elementary energy process unit?

Read Chapter 3 pp. 123-132 (energy balances)

EngrD 2190 – Lecture 11

Homework 3 due today at noon.

Write team code and names of all *contributing* team members on all solutions. Indicate this week's Team Coordinator.

Submit *after* lecture or deliver to the EngrD 2190 mailbox in a cabinet in the hallway between 130 and 132 Olin Hall. **Not to my mailbox.**

EngrD 2190 – Lecture 11

- Homework 4 due Friday 9/26:

Formal mass balances on processes with chemical reactions:

exercises 3.33 and 3.43

Append a list of 'take-aways' to each exercise.

Every equation must have an explicit source.

Process Design with qualitative, informal mass balances:

exercises 3.119 and 3.124

Append a list of 'take-aways' to each exercise.

Requirements for Formal Mass Balances

- Define nomenclature.
- Show system borders and state assumptions.
- State source of equations. *Every equation must have an explicit source.*
examples: “apply conservation of mass” or “stream compositions”
or “process specification for washer”
- Describe derivation. “Substitute eqns (1) and (2) into eqn (3).”
- Box your answers. Numbers must have proper significant figures
and include units (e.g., kg/min).

Flow sheets for mass balance exercises are posted on-line.
Select the “Textbook” item at the EngrD 2190 homepage.

Homework 2 Excellence – Exercise 2.23 – Team 11

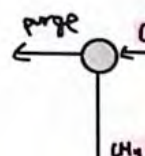
PROBLEM 2.23 B

TEAM 11

Isabelle Bennie

Week coordinator: Steffanie Jones

Anna Voronova

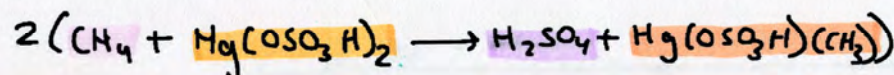


CH_4 (excess)

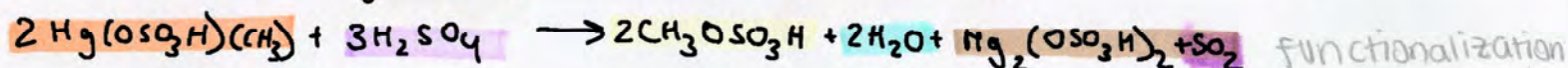
← purge
make-up H_2SO_4

make-up
 $\text{Hg}(\text{OSO}_3\text{H})_2$

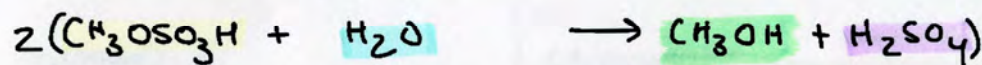
O_2 O_2



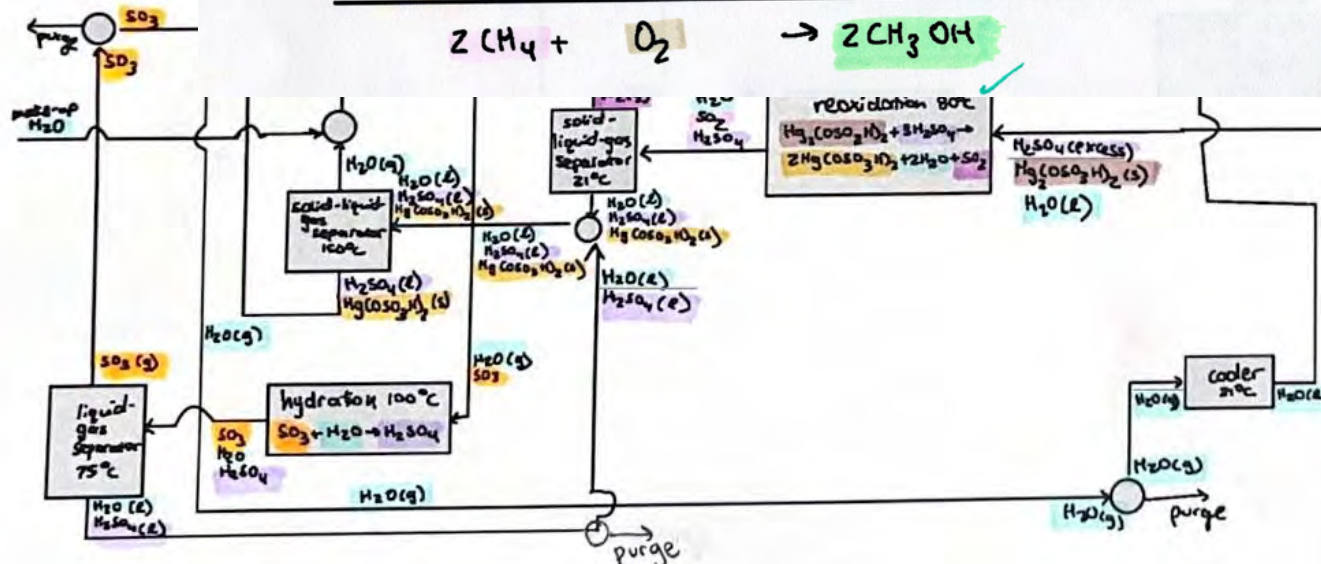
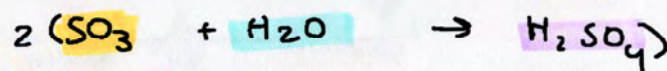
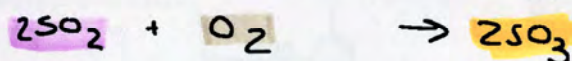
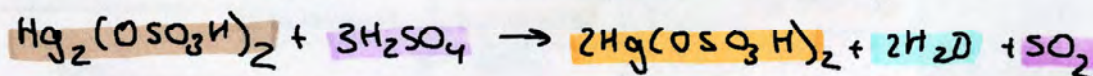
activation



functionalization



hydrolysis
reoxidation
oxidation
hydration



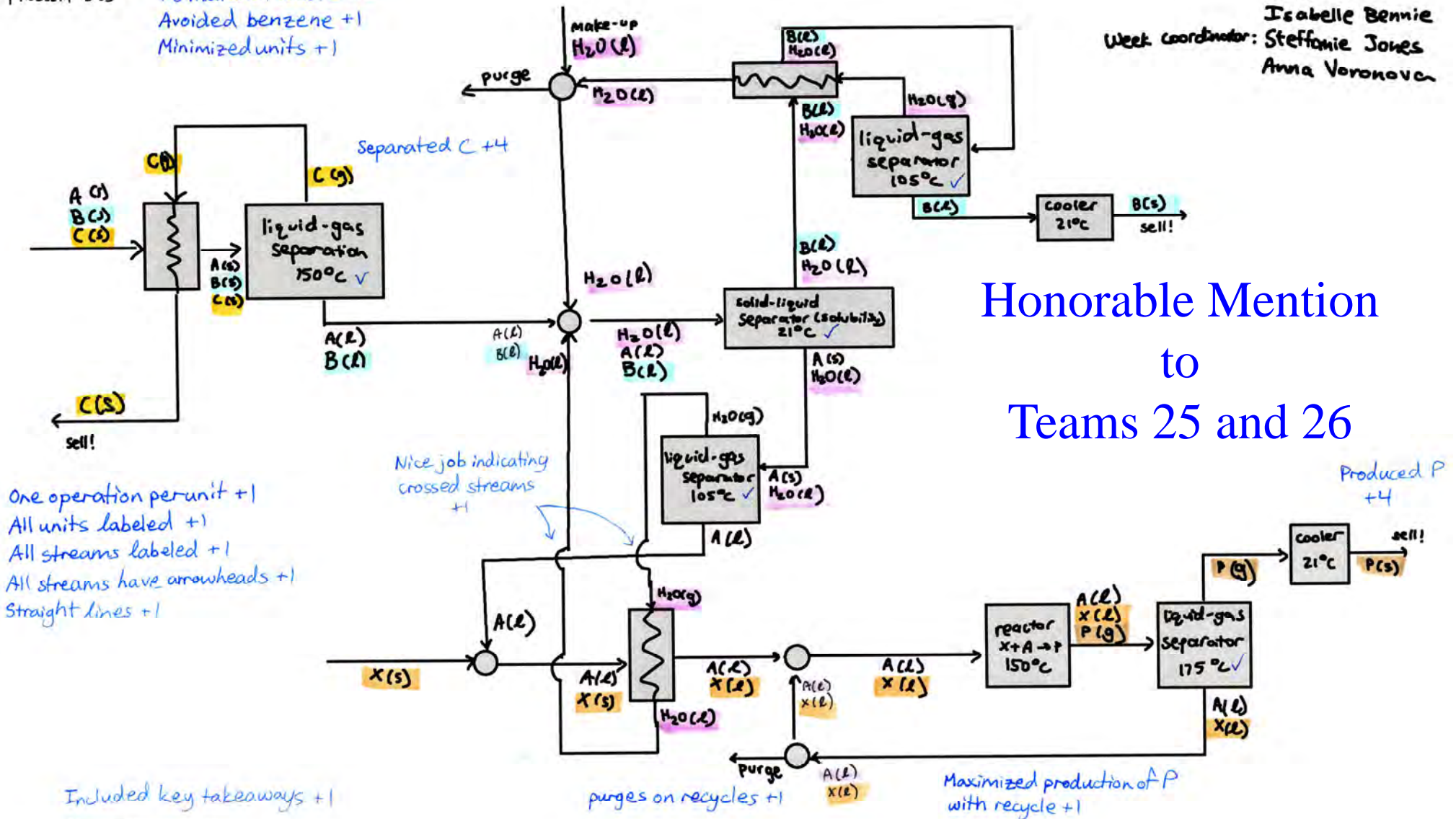
Honorable Mention
to
Teams 6, 13, and 18

Homework 2 Excellence – Exercise 2.33 – Team 11

PROBLEM 2.33

Correct separator temperatures +3
Used heat exchangers to minimize wasted energy +1
No material waste +2
Avoided benzene +1
Minimized units +1

TEAM 11
Isabelle Bennie
Week coordinator: Steffanie Jones
Anna Voronova



Honorable Mention
to
Teams 25 and 26

One operation per-unit +1
All units labeled +1
All streams labeled +1
All streams have arrowheads +1
Straight lines +1

Included key takeaways +1

Key Takeaways:

1. Heat exchangers can greatly reduce the amount of energy needed for a process
2. It is easiest to sell solids.
3. Solubility separators can be useful when liquid-gas separators are not feasible or more energetically taxing.

Mathematical Modeling

Translate a physical and chemical description into equations.

Part 1. Mass Balances

Universal Laws

Conservation of Mass

$$F_{T,\text{in}} = F_{T,\text{out}}$$

must define system borders

Process Specifications

5% ~~of~~ the recycle ~~is~~ purged $\Rightarrow 0.05 \times F_{T,\text{recycle}} = F_{T,\text{purge}}$

\times $=$

Part 2. Energy Balances

Universal Laws

Conservation of Energy

$$q_{\text{in}} = q_{\text{out}}$$

Constitutive 'Laws'

$$\left. \begin{aligned} \Delta q &= F_T C_P (T_{\text{out}} - T_{\text{in}}) \\ \Delta q &= F_T (\Delta H_{\text{phase}}) \end{aligned} \right\} \begin{array}{l} \text{from classical} \\ \text{thermodynamics} \end{array}$$

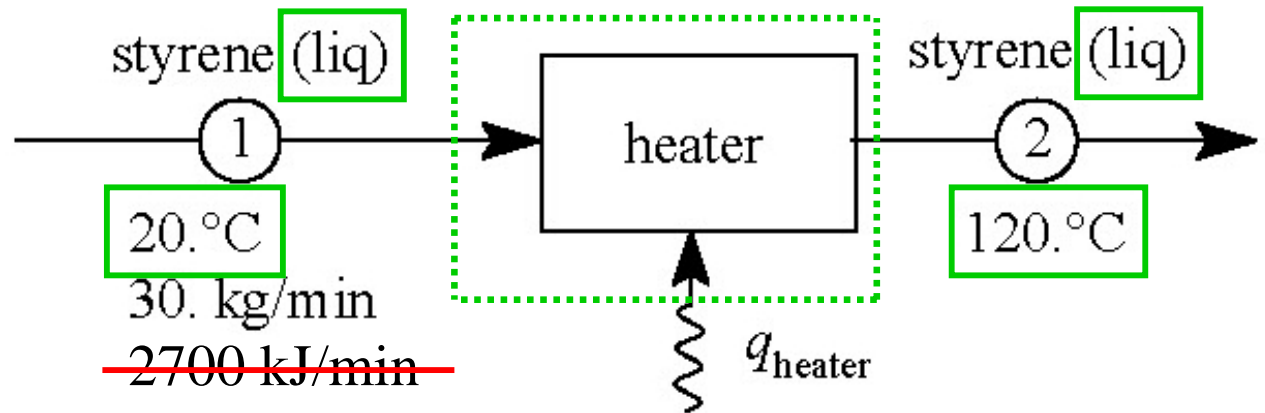
phenomenological; from empirical relations, not from basic principles

Part 3. \$ Balances

Energy Balance Example 1

energy indicators: phase and temperature

Example 1. Calculate q_{heater} .



Cannot specify absolute energy flow rates.

Can only specify *differences* between energy flow rates.

Cannot measure differences between energy flow rates.

Must measure energy indicators and calculate energy differences.

Applying an Energy Balance

Define $q_i \equiv$ flow rate of energy in stream i (kJ/min)

Apply the Conservation of Energy

rate of energy in = rate of energy out

$$q_1 + q_{\text{heater}} = q_2$$

Shorthand for

1. steady state (in = out)

2. system with green borders

$q_1 = ?$ Use an ‘energy meter’ on stream 1? No. Does not exist.

We can measure the mass of a stream,
but we cannot measure the energy of a stream.

Must use energy indicators. Temperature!

How to convert T to q ? Thermodynamics!

(change in internal energy) \propto (mass) \times (change in temperature) for $\Delta P = 0$

$$\Delta U = (\text{mass}) \times C_P \times \Delta T$$

proportionality constant – heat capacity

“constant” is not constant – changes with substance
– changes with T and P

Applying an Energy Balance, cont'd

$$\Delta U = (\text{mass}) \times C_p \times \Delta T$$

Divide both sides by time

$$\frac{\Delta U}{\text{time}} = \frac{\text{mass}}{\text{time}} \times \bar{C}_p \times \Delta T$$

$$\Delta q = F \bar{C}_p (\Delta T) \quad \text{equation 3.114}$$

Note: we do *not* have an equation for $q = \dots$ We must group q 's into Δq 's

Return to the energy balance on the heater.

rate of energy in = rate of energy out

$$q_1 + q_{\text{heater}} = q_2$$

Group q 's into connected mass streams:

$$q_{\text{heater}} = \underbrace{q_2 - q_1}_{\Delta q_{1 \rightarrow 2}}$$

streams 1 and 2 are same substance: styrene

streams 1 and 2 have same flow rate: 100 kg/min

q difference arranged as 'out' minus 'in'

Applying an Energy Balance, cont'd

$$q_{\text{heater}} = \Delta q_{1 \rightarrow 2}$$

Use thermodynamics to substitute for Δq .

$$q_{\text{heater}} = F_{T,1} \bar{C}_{P,\text{styrene}} (T_2 - T_1)$$

assumes C_p is independent of T

Calculate a numerical value. *Include explicit units.*

see data on p. 200

$$q_{\text{heater}} = \left(\frac{30 \text{ kg styrene}}{\text{min}} \right) \left(\frac{183 \text{ joules}}{\text{°C} \cdot \text{mol styrene}} \right) (120\text{°C} - 20\text{°C}) \left(\frac{1 \text{ mol styrene}}{104 \text{ g styrene}} \right) \left(\frac{1000 \text{ g}}{1 \text{ kg}} \right)$$

important

$$q_{\text{heater}} = 5.279 \times 10^6 \text{ joules/min}$$

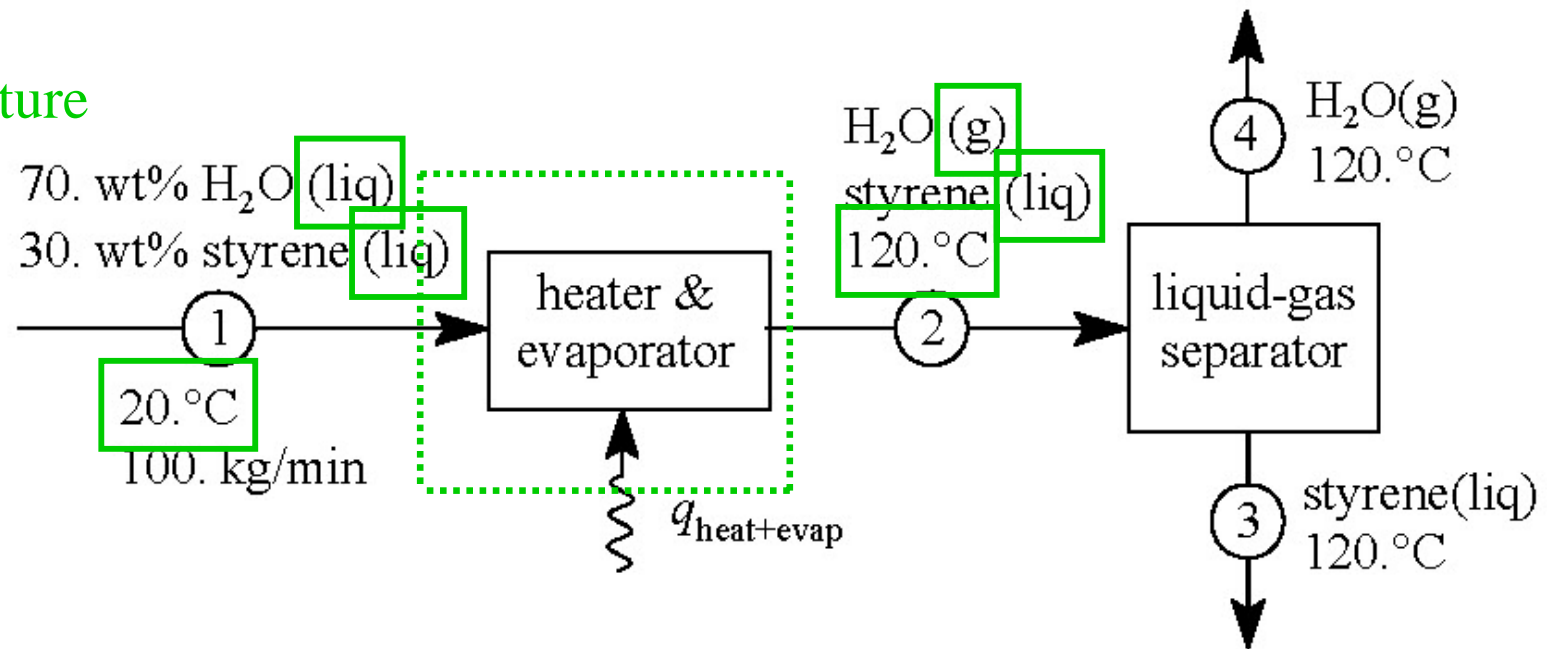
$$q_{\text{heater}} = 5.3 \times 10^3 \text{ kJ/min}$$

Energy Balance Example 2

Example 2: Exercise 3.63(A). Calculate $q_{\text{heat+evap}}$.

Solution is posted.

energy indicators:
phase and temperature



Although the mass balance is simple, the energy balance is complicated.

Heat styrene (liquid) to 120°C.

Heat water (liquid) to 100°C.

Evaporate water (liquid) at 100°C.

Heat steam (vapor) to 120°C.

Strategy: represent heater+evaporator as a system of elementary energy units.

one mass stream in, one mass stream out

one energy change: temperature change

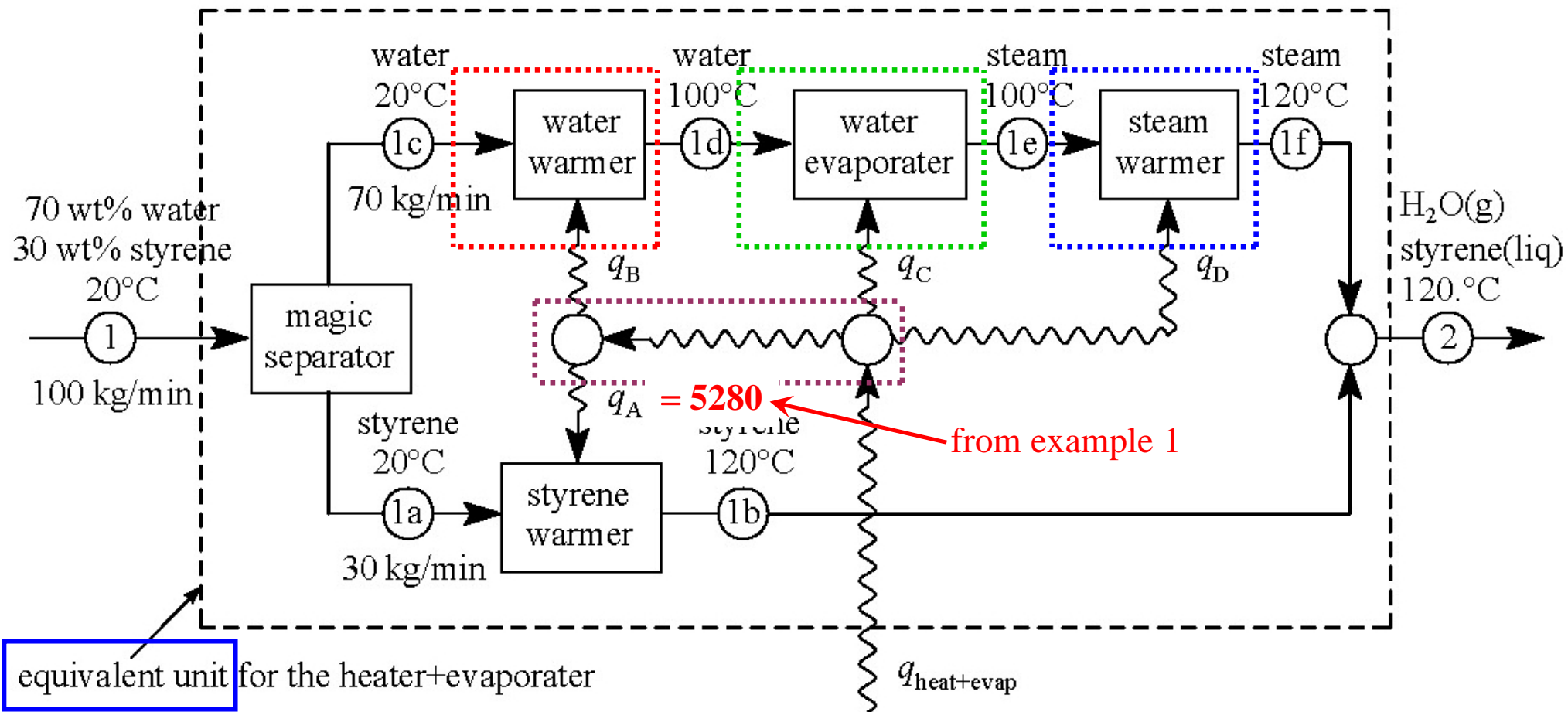
or phase change

or pressure change

or velocity change ...

in later courses

Example 2: Exercise 3.63(A). Equivalent unit for heater+evaporator:



Comprises *elementary* energy units

- one stream in, one stream out.
- one energy change: ΔT or Δphase (EngrD 2190)
 ΔP , Δv , Δheight , etc (later courses)

Example 2: Energy Balance on Heater+Evaporator

Water warmer: rate of energy in = rate of energy out

$$q_{1c} + q_B = q_{1d}$$

Group q 's into Δq 's: $q_B = q_{1d} - q_{1c} = F_{T,1c} \bar{C}_{P,\text{water}} (T_{1d} - T_{1c})$

$$q_B = \left(\frac{70 \text{ kg water}}{\text{min}} \right) \left(\frac{75 \text{ joules}}{^\circ\text{C} \cdot \text{mol water}} \right) (100 - 20^\circ\text{C}) \left(\frac{1000 \text{ mol water}}{18 \text{ kg water}} \right)$$

$$q_B = 23,350 \text{ kJ/min}$$

Evaporator: rate of energy in = rate of energy out

$$q_{1d} + q_C = q_{1e}$$

Group q 's into Δq 's: $q_C = q_{1e} - q_{1d} = \cancel{F_{T,1d} \bar{C}_{P,\text{water}} (T_{1e} - T_{1d})}$
 $= F_{T,1d} \Delta \bar{H}_{\text{vaporization}}$

$$q_C = \left(\frac{70 \text{ kg water}}{\text{min}} \right) \left(\frac{4.1 \times 10^4 \text{ joules}}{\text{mol water}} \right) \left(\frac{1000 \text{ mol water}}{18 \text{ kg water}} \right)$$

$$q_C = 159,600 \text{ kJ/min}$$

Example 2: Energy Balance on Heater+Evaporator, cont'd

Steam warmer: rate of energy in = rate of energy out

$$q_{1e} + q_D = q_{1f}$$

Group q 's into Δq 's: $q_D = q_{1f} - q_{1e} = F_{T,1e} C_{P,\text{steam}} (T_{1f} - T_{1e})$

$$q_D = \left(\frac{70 \text{ kg steam}}{\text{min}} \right) \left(\frac{35 \text{ joules}}{^\circ\text{C} \cdot \text{mol steam}} \right) (120 - 100^\circ\text{C}) \left(\frac{1000 \text{ mol steam}}{18 \text{ kg steam}} \right)$$

$$q_D = 2720 \text{ kJ/min}$$

Combine the energy flows to the elementary energy units.

Write an energy balance on a fictitious energy combiner.

rate of energy in = rate of energy out

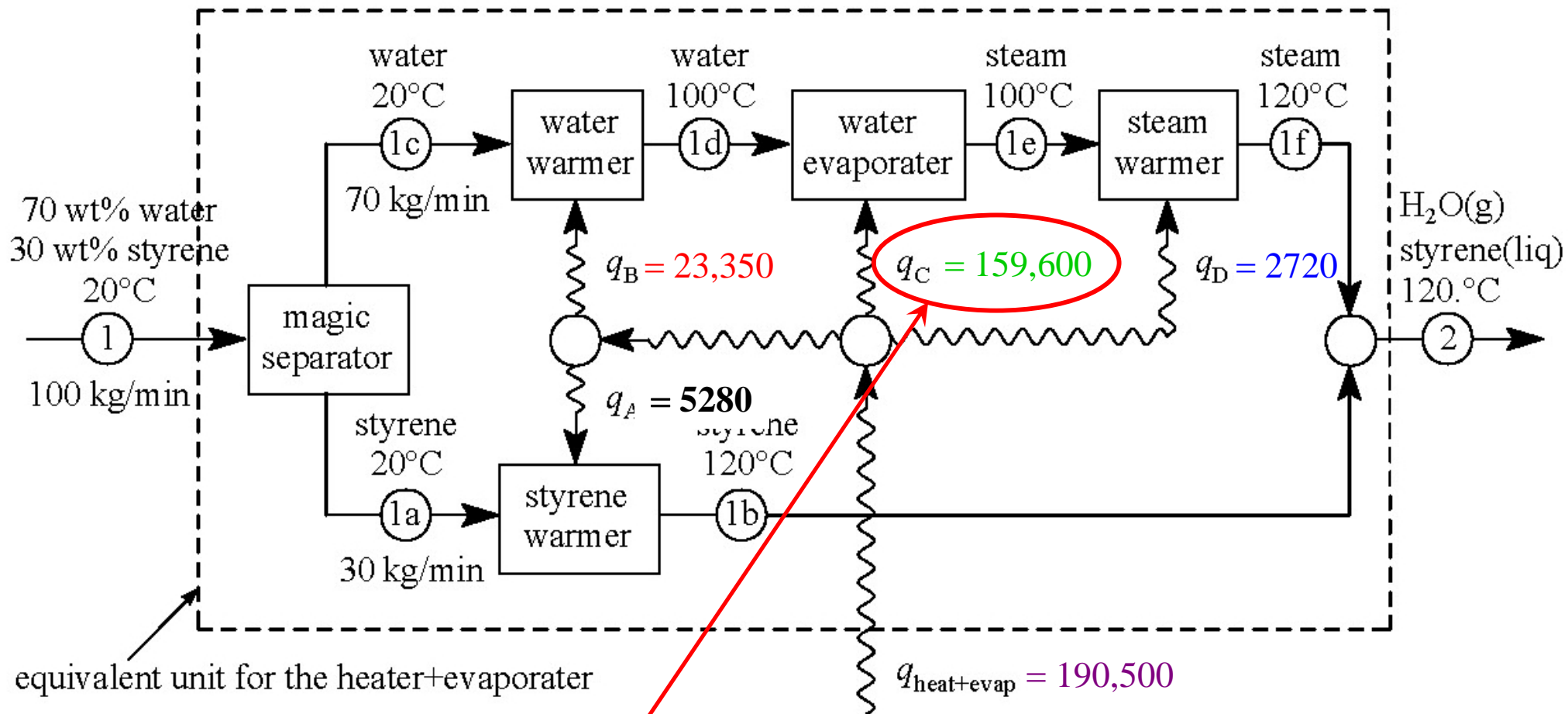
$$q_{\text{heater+evaporator}} = q_A + q_B + q_C + q_D$$

$$q_{\text{heater+evaporator}} = 5280 + 23,350 + 159,600 + 2720$$

$$q_{\text{heater+evaporator}} = 190,950 \text{ kJ/min}$$

$$q_{\text{heater+evaporator}} = 1.91 \times 10^5 \text{ kJ/min}$$

Example 2: Exercise 3.63(A). Equivalent unit for heater+evaporator:



Important: evaporating the water is the major energy use.

Best source of energy to recover in a heat exchanger (Example 3)

Defining Question: What is an elementary energy process unit?

Answer: An elementary energy process unit is a fictitious unit to represent a single energy change for a single mass stream.

An elementary energy process unit has –
one stream in and one stream out, and
exactly one energy change – a temperature change, or
a phase change, or
in later courses ↓ a velocity change, or
a pressure change, or
a height change, or ...

*Replace a complex energy unit with an Equivalent Unit
that comprises elementary energy process units.*

Bring Today's Lecture Handout to Monday's Lecture.