

EngrD 2190 – Lecture 11

Concept: Process Analysis – Mathematical Modeling with Energy Balances

- One cannot measure energy; one must use measurable quantities (temperature and phase) and convert to energy.
- One cannot calculate absolute energy; one must calculate energy *change*.

Context: A heater, a heater + partial evaporator, and a heat exchanger.

Defining Question: What is an elementary energy process unit?

Read Chapter 3 pp. 123-132 (energy balances)

EngrD 2190 – Lecture 11

Homework 3 due today at noon.

Write team code and names of all *contributing* team members on all solutions.
Indicate this week's Team Coordinator.

Submit *after* lecture or deliver to the EngrD 2190 mailbox in a cabinet
in the hallway between 130 and 132 Olin Hall. **Not to my mailbox.**

EngrD 2190 – Lecture 11

- Homework 4 due Friday 9/26:

Formal mass balances on processes with chemical reactions:

exercises 3.33 and 3.43

Append a list of ‘take-aways’ to each exercise.

Every equation must have an explicit source.

Process Design with qualitative, informal mass balances:

exercises 3.119 and 3.124

Append a list of ‘take-aways’ to each exercise.

Requirements for Formal Mass Balances

- Define nomenclature.
- Show system borders and state assumptions.
- State source of equations. *Every equation must have an explicit source.*
examples: “apply conservation of mass” or “stream compositions”
or “process specification for washer”
- Describe derivation. “Substitute eqns (1) and (2) into eqn (3).”
- Box your answers. Numbers must have proper significant figures
and include units (e.g., kg/min).

Flow sheets for mass balance exercises are posted on-line.

Select the “Textbook” item at the EngrD 2190 homepage.

Homework 2 Excellence – Exercise 2.23 – Team 11

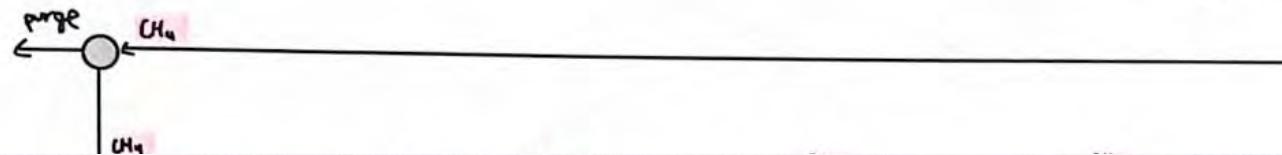
PROBLEM 2.23 B

TEAM 11

Isabelle Bennie

Week coordinator: Steffanie Jones

Anna Voronova



CH_4 (excess)

← purge
make-up H_2S

$$2(\text{NH}_4 + \text{Hg}(\text{OSO}_3\text{H})_2 \rightarrow \text{H}_2\text{SO}_4 + \text{Hg}(\text{OSO}_3\text{H})(\text{CH}_3))$$

activation

make-up H_2S

$$2 \text{ (CH}_3\text{OSO}_3\text{H} + \text{ H}_2\text{O} \longrightarrow (\text{CH}_3\text{OH} + \text{H}_2\text{SO}_4)$$

O₂ functionalization

$$\text{Hg}_2(\text{OSO}_3\text{H})_2 + 3\text{H}_2\text{SO}_4 \rightarrow 2\text{Hg}(\text{OSO}_3\text{H})_2 + 2\text{H}_2\text{O} + \text{SO}_2$$

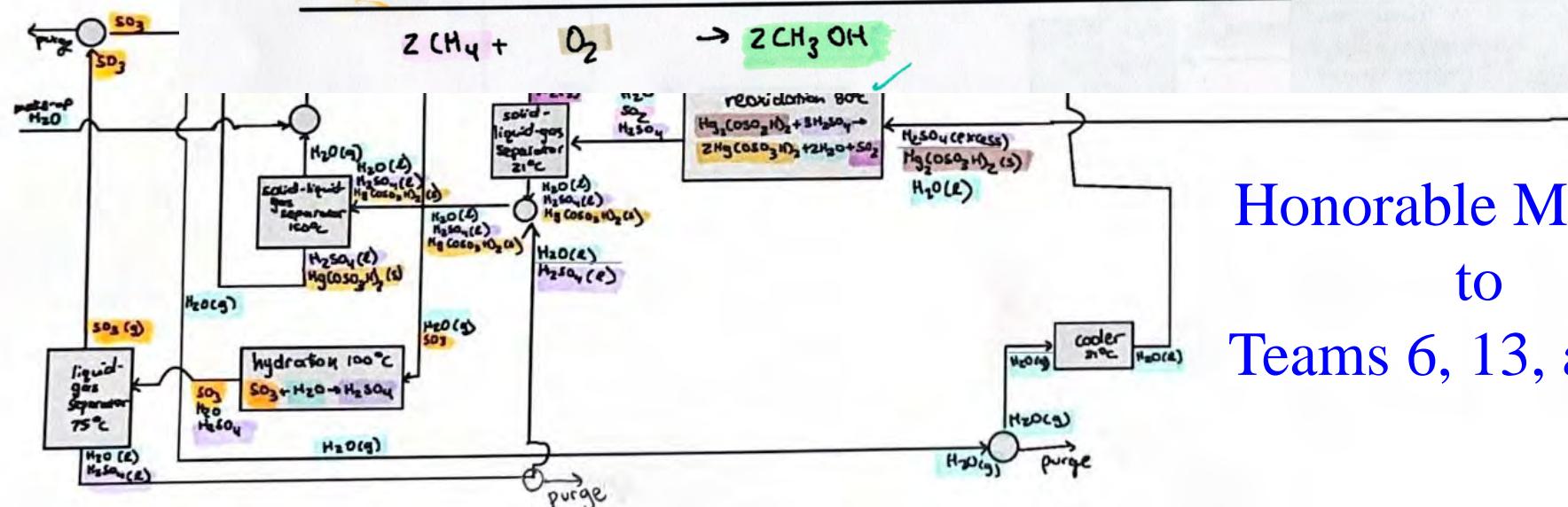
hydrolysis

$$2\text{SO}_2 + \text{O}_2 \rightarrow 2\text{SO}_3$$

reoxidation

$$2 \text{ (SO}_3 + \text{ H}_2\text{O} \rightarrow \text{ H}_2\text{SO}_4)$$

hydration



Honorable Mention to Teams 6, 13, and 18

Homework 2 Excellence – Exercise 2.33 – Team 11

PROBLEM 2.33

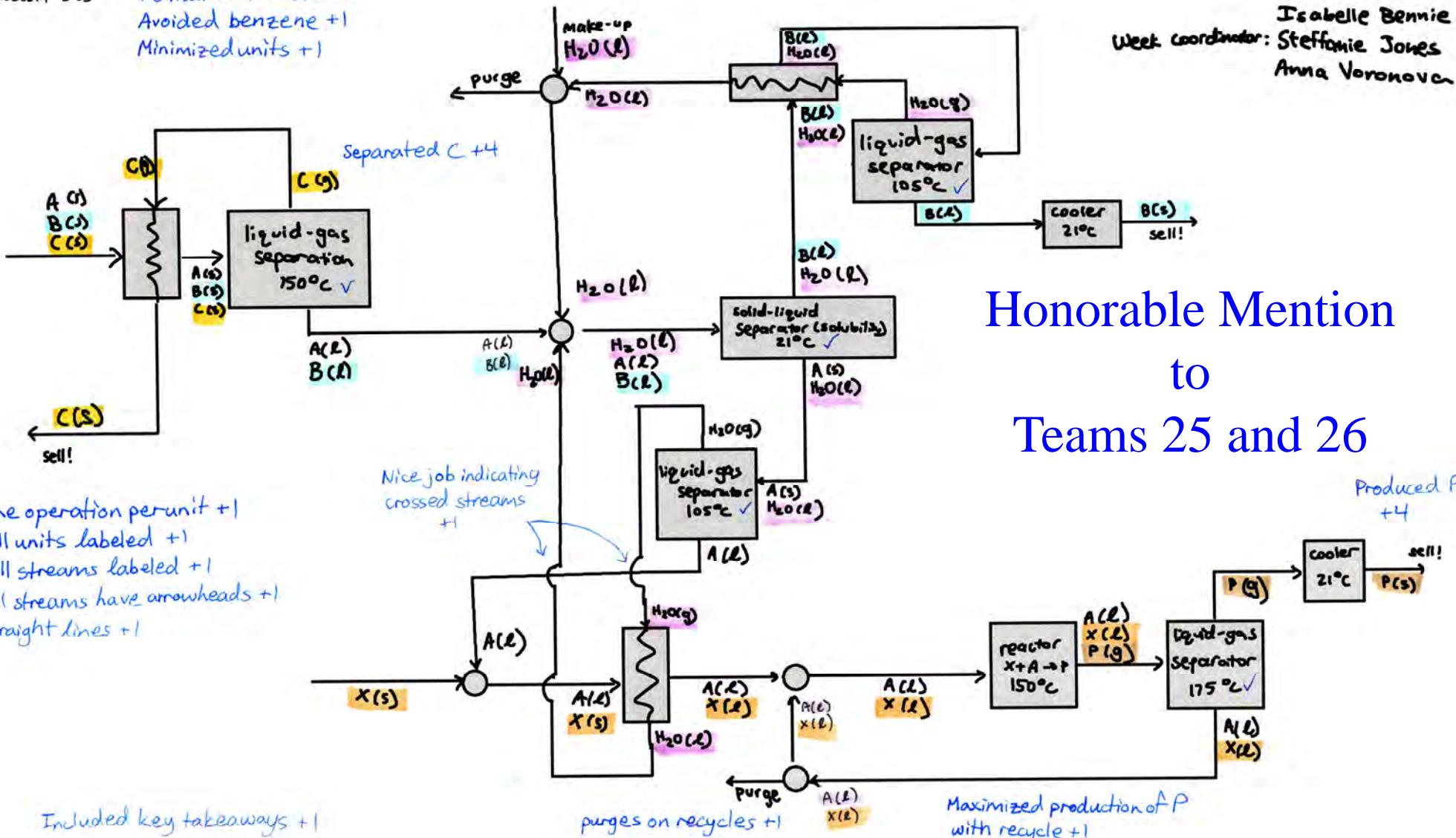
Correct separator temperatures +3

Used heat exchangers to minimize wasted energy +1

No material waste +2

Avoided benzene +1

Minimized units +1



Honorable Mention
to
Teams 25 and 26

Key Takeaways:

1. Heat exchangers can greatly reduce the amount of energy needed for a process
2. It is easiest to sell solids.
3. Solubility separators can be useful when liquid-gas separators are not feasible or more energetically taxing.

Mathematical Modeling

Translate a physical and chemical description into equations.

Part 1. Mass Balances

Universal Laws

Conservation of Mass

$$F_{T,in} = F_{T,out}$$

must define system borders

Process Specifications

$$5\% \text{ of the recycle} \times \text{is purged} = 0.05 \times F_{T,recycle} = F_{T,purge}$$

Part 2. Energy Balances

Universal Laws

Conservation of Energy

$$q_{in} = q_{out}$$

Constitutive 'Laws'

$$\Delta q = F_T C_P (T_{out} - T_{in})$$
$$\Delta q = F_T (\Delta H_{phase})$$

} from classical
thermodynamics

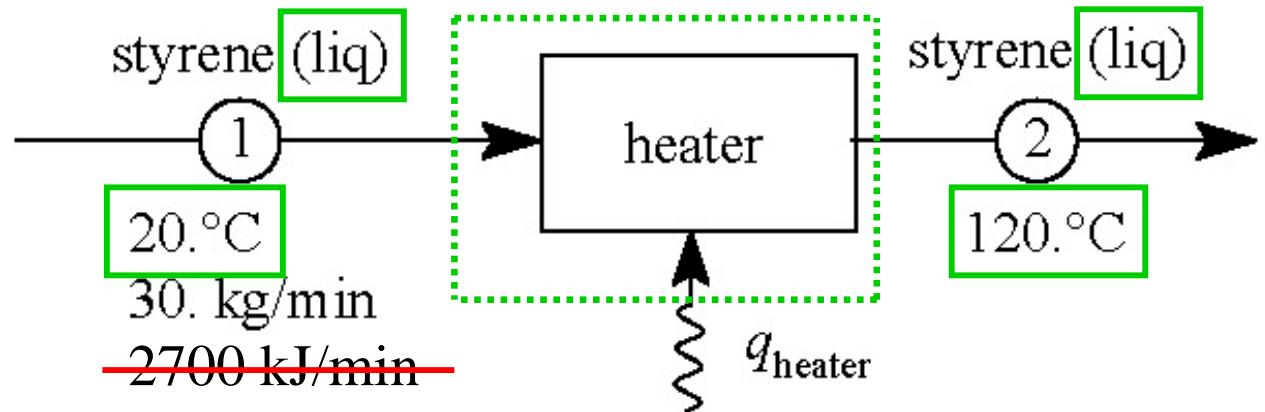
phenomenological; from empirical relations, not from basic principles

Part 3. \$ Balances

Energy Balance Example 1

Example 1. Calculate q_{heater} .

energy indicators: phase and temperature



Cannot specify absolute energy flow rates.

Can only specify *differences* between energy flow rates.

Cannot measure differences between energy flow rates.

Must measure energy indicators and calculate energy differences.

Applying an Energy Balance

Define $q_i \equiv$ flow rate of energy in stream i (kJ/min)

Apply the Conservation of Energy

rate of energy in = rate of energy out

$$q_1 + q_{\text{heater}} = q_2$$

Shorthand for

1. steady state (in = out)
2. system with green borders

$q_1 = ?$ Use an ‘energy meter’ on stream 1? No. Does not exist.

We can measure the mass of a stream,
but we cannot measure the energy of a stream.

Must use energy indicators. Temperature!

How to convert T to q ? Thermodynamics!

(change in internal energy) \propto (mass) \times (change in temperature) for $\Delta P = 0$

$$\Delta U = (\text{mass}) \times C_p \times \Delta T$$

proportionality constant – heat capacity

“constant” is not constant – changes with substance
– changes with T and P

Applying an Energy Balance, cont'd

$$\Delta U = (\text{mass}) \times C_P \times \Delta T$$

Divide both sides by time $\frac{\Delta U}{\text{time}} = \frac{\text{mass}}{\text{time}} \times \bar{C}_P \times \Delta T$

$$\Delta q = F \bar{C}_P (\Delta T) \quad \text{equation 3.114}$$

Note: we do *not* have an equation for $q = \dots$ We must group q 's into Δq 's

Return to the energy balance on the heater.

$$\text{rate of energy in} = \text{rate of energy out}$$

$$q_1 + q_{\text{heater}} = q_2$$

Group q 's into connected mass streams:

$$q_{\text{heater}} = \underbrace{q_2 - q_1}_{\Delta q_{1 \rightarrow 2}} = \Delta q_{1 \rightarrow 2}$$

streams 1 and 2 are same substance: styrene

streams 1 and 2 have same flow rate: 100 kg/min

q difference arranged as 'out' minus 'in'

Applying an Energy Balance, cont'd

$$q_{\text{heater}} = \Delta q_{1 \rightarrow 2}$$

Use thermodynamics to substitute for Δq .

$$q_{\text{heater}} = F_{T,1} \bar{C}_{P,\text{styrene}} (T_2 - T_1)$$

assumes C_P is independent of T

Calculate a numerical value. *Include explicit units.*

$$q_{\text{heater}} = \left(\frac{30 \text{ kg styrene}}{\text{min}} \right) \left(\frac{183 \text{ joules}}{\text{}^{\circ}\text{C} \cdot \text{mol styrene}} \right) (120 \text{ }^{\circ}\text{C} - 20 \text{ }^{\circ}\text{C}) \left(\frac{1 \text{ mol styrene}}{104 \text{ g styrene}} \right) \left(\frac{1000 \text{ g}}{1 \text{ kg}} \right)$$

see data on p. 200

important

$$q_{\text{heater}} = 5.279 \times 10^6 \text{ joules/min}$$

$$q_{\text{heater}} = 5.3 \times 10^3 \text{ kJ/min}$$

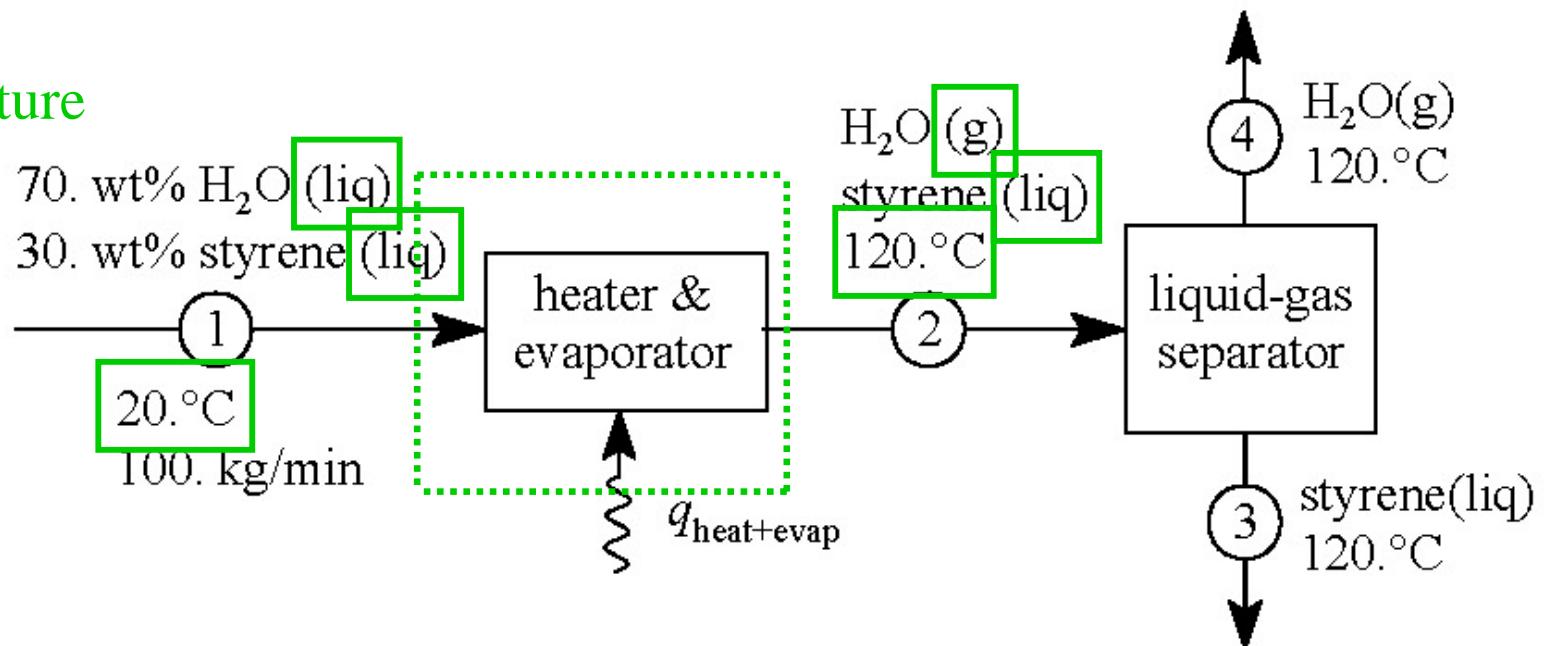
Energy Balance Example 2

Example 2: Exercise 3.63(A). Calculate $q_{\text{heat+evap}}$.

Solution is posted.

energy indicators:

phase and temperature



Although the mass balance is simple, the energy balance is complicated.

Heat styrene (liquid) to 120°C.

Heat water (liquid) to 100°C.

Evaporate water (liquid) at 100°C.

Heat steam (vapor) to 120°C.

Strategy: represent heater+evaporator as a system of elementary energy units.

one mass stream in, one mass stream out

one energy change: temperature change

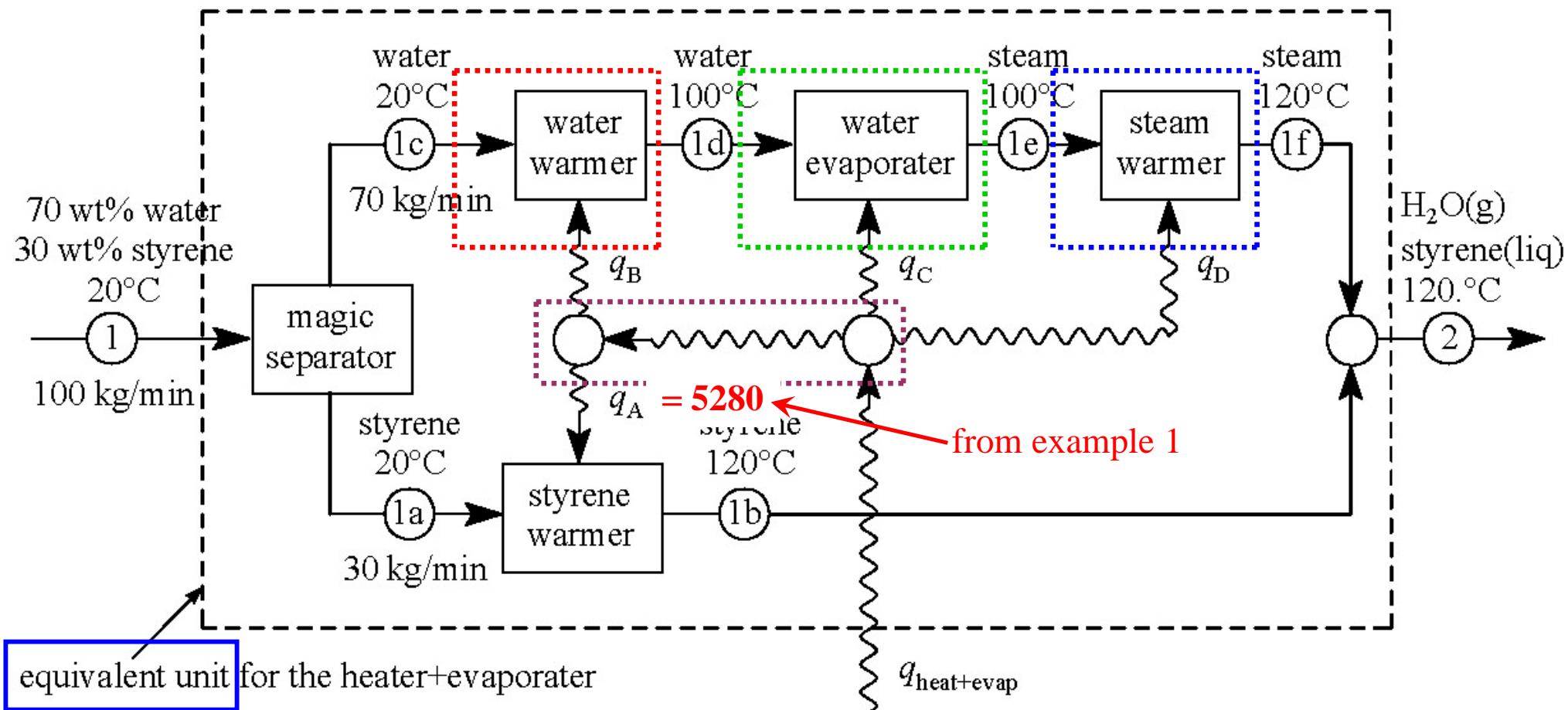
or phase change

or pressure change

in later courses

or velocity change ...

Example 2: Exercise 3.63(A). Equivalent unit for heater+evaporator:



Comprises *elementary* energy units

- one stream in, one stream out.
- one energy change: ΔT or Δ phase (EngrD 2190)
 ΔP , Δv , Δ height, etc (later courses)

Example 2: Energy Balance on Heater+Evaporator

Water warmer: rate of energy in = rate of energy out

$$q_{1c} + q_B = q_{1d}$$

Group q 's into Δq 's:
$$q_B = q_{1d} - q_{1c} = F_{T,1c} \bar{C}_{P, \text{water}} (T_{1d} - T_{1c})$$

$$q_B = \left(\frac{70 \text{ kg water}}{\text{min}} \right) \left(\frac{75 \text{ joules}}{\text{ }^\circ\text{C} \cdot \text{mol water}} \right) (100 - 20 \text{ }^\circ\text{C}) \left(\frac{1000 \text{ mol water}}{18 \text{ kg water}} \right)$$

$$q_B = 23,350 \text{ kJ/min}$$

Evaporator: rate of energy in = rate of energy out

$$q_{1d} + q_C = q_{1e}$$

Group q 's into Δq 's:
$$q_C = q_{1e} - q_{1d} = \cancel{F_{T,1d} \bar{C}_{P, \text{water}} (T_{1c} - T_{1d})}$$

$$= F_{T,1d} \Delta \bar{H}_{\text{vaporization}}$$

$$q_C = \left(\frac{70 \text{ kg water}}{\text{min}} \right) \left(\frac{4.1 \times 10^4 \text{ joules}}{\text{mol water}} \right) \left(\frac{1000 \text{ mol water}}{18 \text{ kg water}} \right)$$

$$q_C = 159,600 \text{ kJ/min}$$

Example 2: Energy Balance on Heater+Evaporator, cont'd

Steam warmer: rate of energy in = rate of energy out

$$q_{1e} + q_D = q_{1f}$$

Group q 's into Δq 's: $q_D = q_{1f} - q_{1e} = F_{T,1e} C_{P,steam} (T_{1f} - T_{1e})$

$$q_D = \left(\frac{70 \text{ kg steam}}{\text{min}} \right) \left(\frac{35 \text{ joules}}{\text{ }^\circ\text{C} \cdot \text{mol steam}} \right) (120 - 100 \text{ }^\circ\text{C}) \left(\frac{1000 \text{ mol steam}}{18 \text{ kg steam}} \right)$$

$$q_D = 2720 \text{ kJ/min}$$

Combine the energy flows to the elementary energy units.

Write an energy balance on a fictitious energy combiner.

rate of energy in = rate of energy out

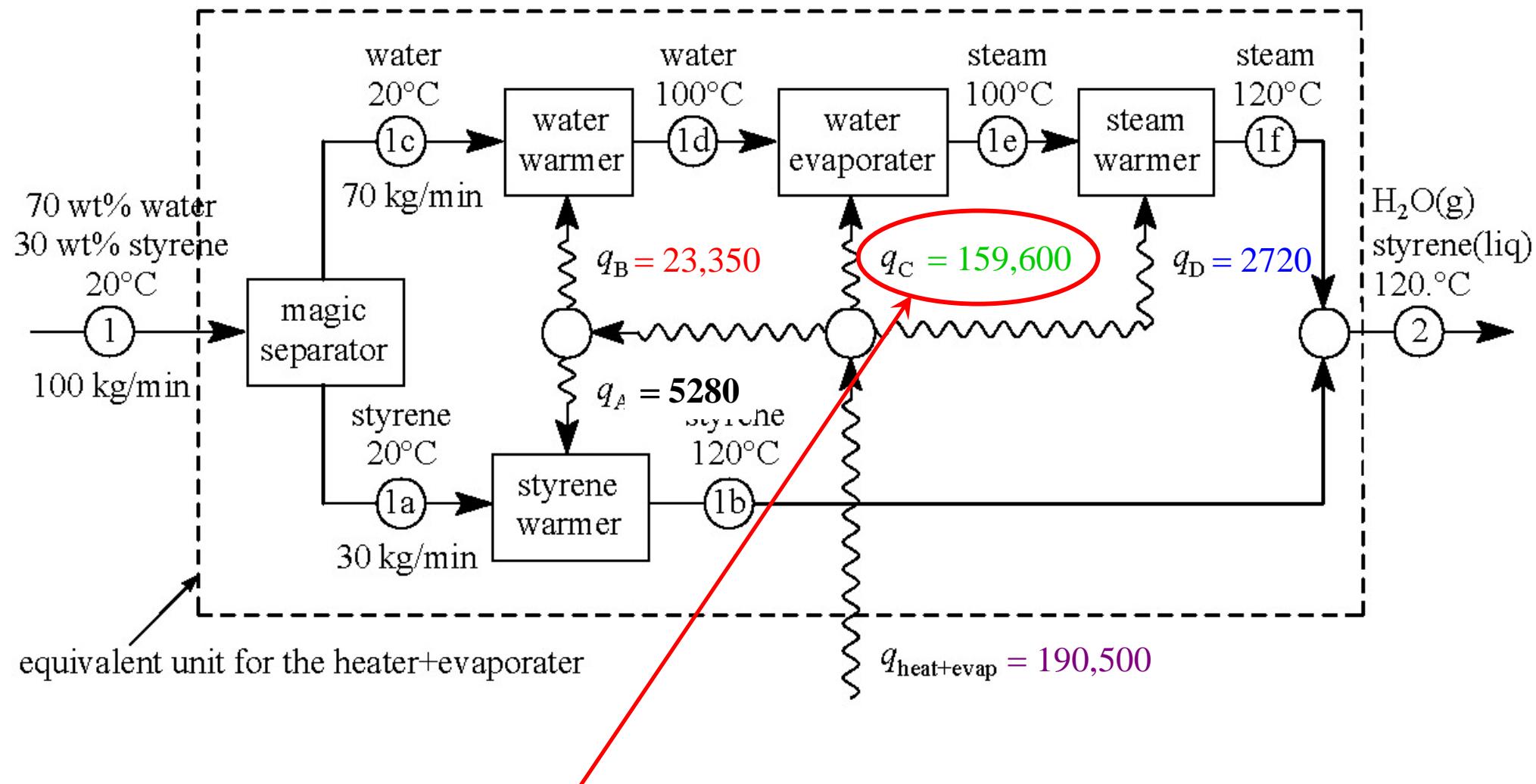
$$q_{\text{heater+evaporator}} = q_A + q_B + q_C + q_D$$

$$q_{\text{heater+evaporator}} = 5280 + 23,350 + 159,600 + 2720$$

$$q_{\text{heater+evaporator}} = 190,950 \text{ kJ/min}$$

$$q_{\text{heater+evaporator}} = 1.91 \times 10^5 \text{ kJ/min}$$

Example 2: Exercise 3.63(A). Equivalent unit for heater+evaporator:



Important: evaporating the water is the major energy use.

Best source of energy to recover in a heat exchanger (Example 3)

Defining Question: What is an elementary energy process unit?

Answer: An elementary energy process unit is a fictitious unit to represent a single energy change for a single mass stream.

An elementary energy process unit has –
one stream in and one stream out, and
exactly one energy change – a temperature change, or
a phase change, or
in later courses a velocity change, or
a pressure change, or
a height change, or ...

*Replace a complex energy unit with an Equivalent Unit
that comprises elementary energy process units.*

Bring Today's Lecture Handout to Monday's Lecture.