

# EngrD 2190 – Lecture 24

Concept: Graphical Mass Balances – Operating Lines

Context: Multi-Stage Countercurrent Absorbers

Defining Question: What is an operating line?

*Bring a Straightedge or Ruler to Lecture 25.*

# Prelim 2

- Prelim 2: TOMORROW 10/30, 7:30-9:30 p.m., 245 and 128 Olin Hall

Mathematical Modeling:

energy balances and process economics

mass balances on spreadsheets

Graphical Modeling:

graphical energy balances: energy lines.

flash drums:  $T$ -( $x,y$ ) and  $P$ -( $x,y$ ) phase maps.

Design using single-stage units ( $L$ - $V$ ,  $L$ - $L$ , and  $S$ - $L$  separators)

with  $T$ -( $x,y$ ) and  $P$ -( $x,y$ ) phase maps.

Open notes and open exercise solutions.

Bring a calculator and a ruler. Graphing calculators are allowed.

- Practice exercises: 3.74, 3.76, and 3.79 – energy balances  
3.96, 3.97, and 3.99 – process economics  
4.3, 4.7, and 4.88 – graphical energy balances  
4.89 and 4.90 – design with flash drums

*Solutions are posted.*

# Prelim 2

## Grading Rubric for Formal Graphical Model.

### Validity of graphical model

16 points

translated process and mathematical equations to points and lines.

(list of 8 specific features of the graphical model)

### Style of graphical model.

4 points

*“Everything drawn on the phase map has an explicit source.”*

Straight and horizontal lines for mixing lines

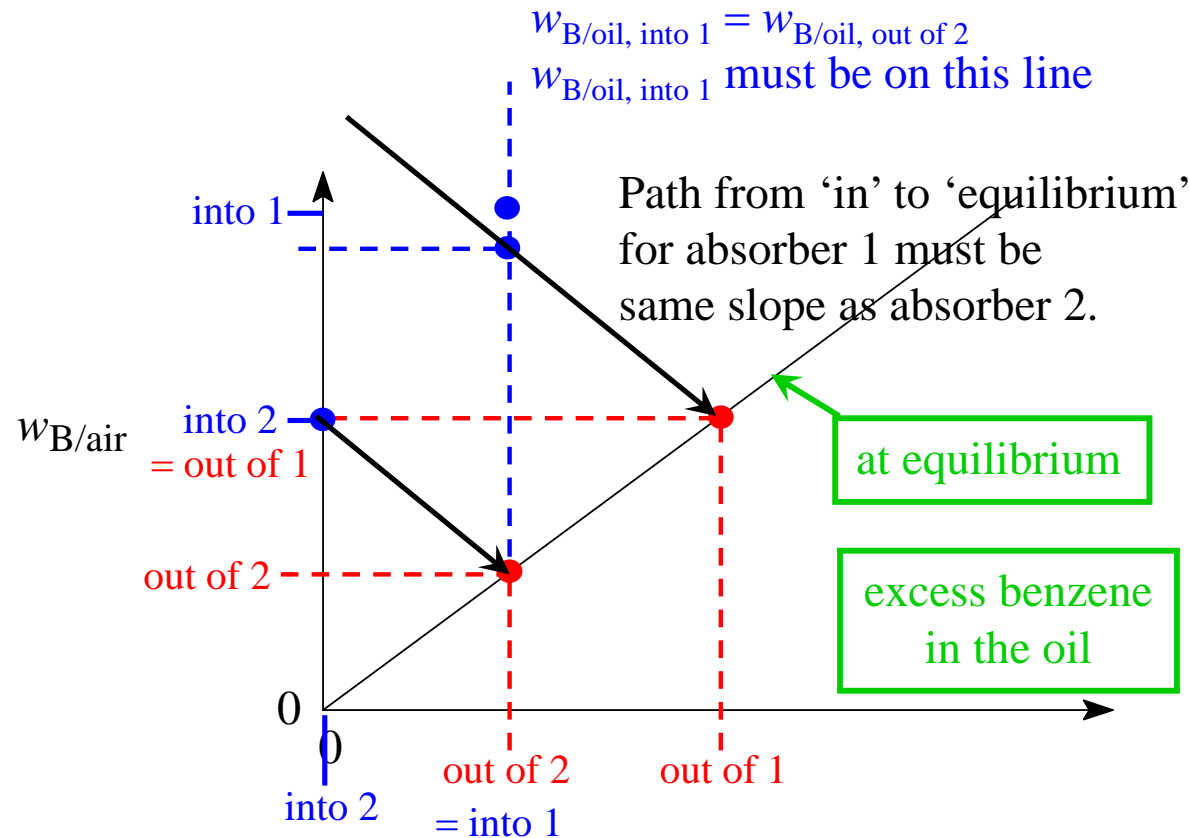
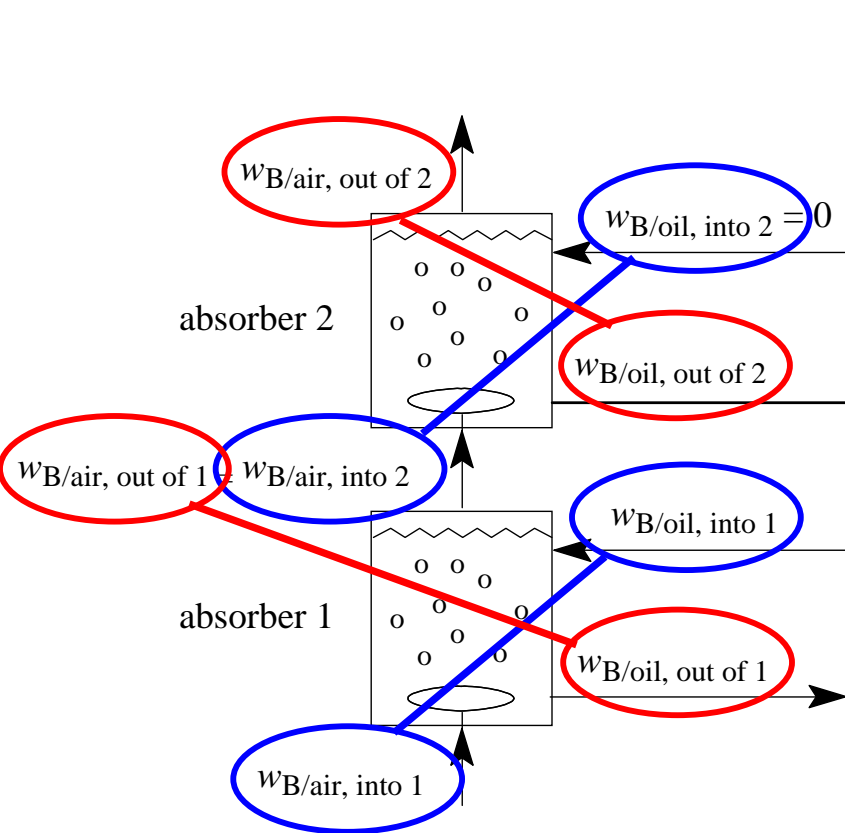
Straight and vertical lines to read numbers on axes.

All streams labeled.

Answer has proper significant figures and correct units.

Constants such as  $C_p$  and  $\Delta H_{\text{melting}}$  and  $\Delta H_{\text{evaporation}}$  should not appear in a graphical modeling analysis.

# Graphical Analysis of a *Better* Two-Stage Absorber: Counter-Current Flow



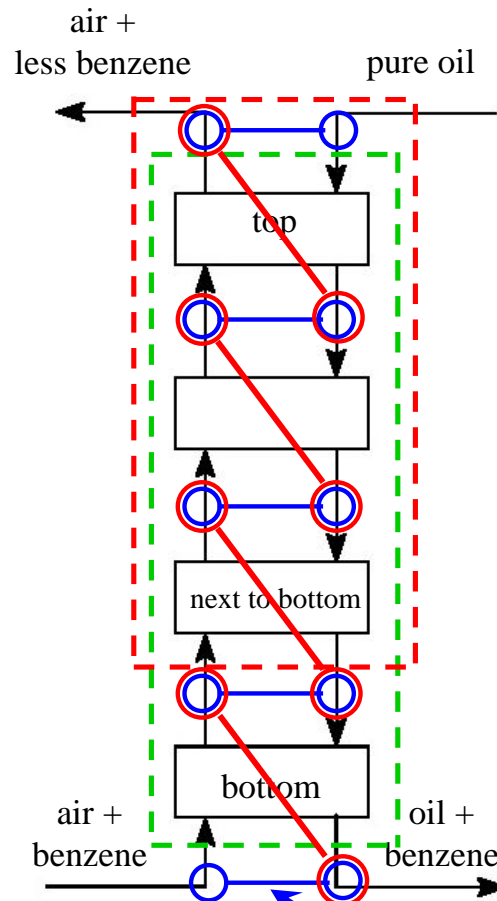
Point for  $(x,y) = (w_{B/oil, \text{ into } 1}, w_{B/air, \text{ into } 1})$  dictated by intersection does not agree with  $w_{B/air, \text{ into } 1}$ .

Must iterate until intersection agrees with  $w_{B/air, \text{ into } 1}$ .

Iteration is tedious for a two-stage absorber. Iteration is unthinkable for a 10-stage absorber.

*There must be a better way ...*

# Graphical Analysis of Multi-Stage Counter-Current Absorbers: A Better Graphical Model.



parameters:

1.  $w_{B/air, in}$
2.  $w_{B/air, out}$
3.  $w_{B/oil, in} = 0$
4.  $w_{B/oil, out}$
5.  $F_{air}$
6.  $F_{oil}$

given

unknown

given

Mass Balance: rate of benzene in = rate of benzene out

(See eqns 4.29 to 4.35, p. 274.)

$$w_{B/air, into bottom} = \left( \frac{F_{oil}}{F_{air}} \right) w_{B/oil, out of bottom} + w_{B/air, out of top}$$

$$y = (\text{slope}) \times x + y \text{ intercept}$$

Adjacent (x,y) pair lies on a line with slope  $F_{oil}/F_{air}$ .

rate of benzene in = rate of benzene out

$$w_{B/air, into next to bottom} = \left( \frac{F_{oil}}{F_{air}} \right) w_{B/oil, out of next to bottom} + w_{B/air, out of top}$$

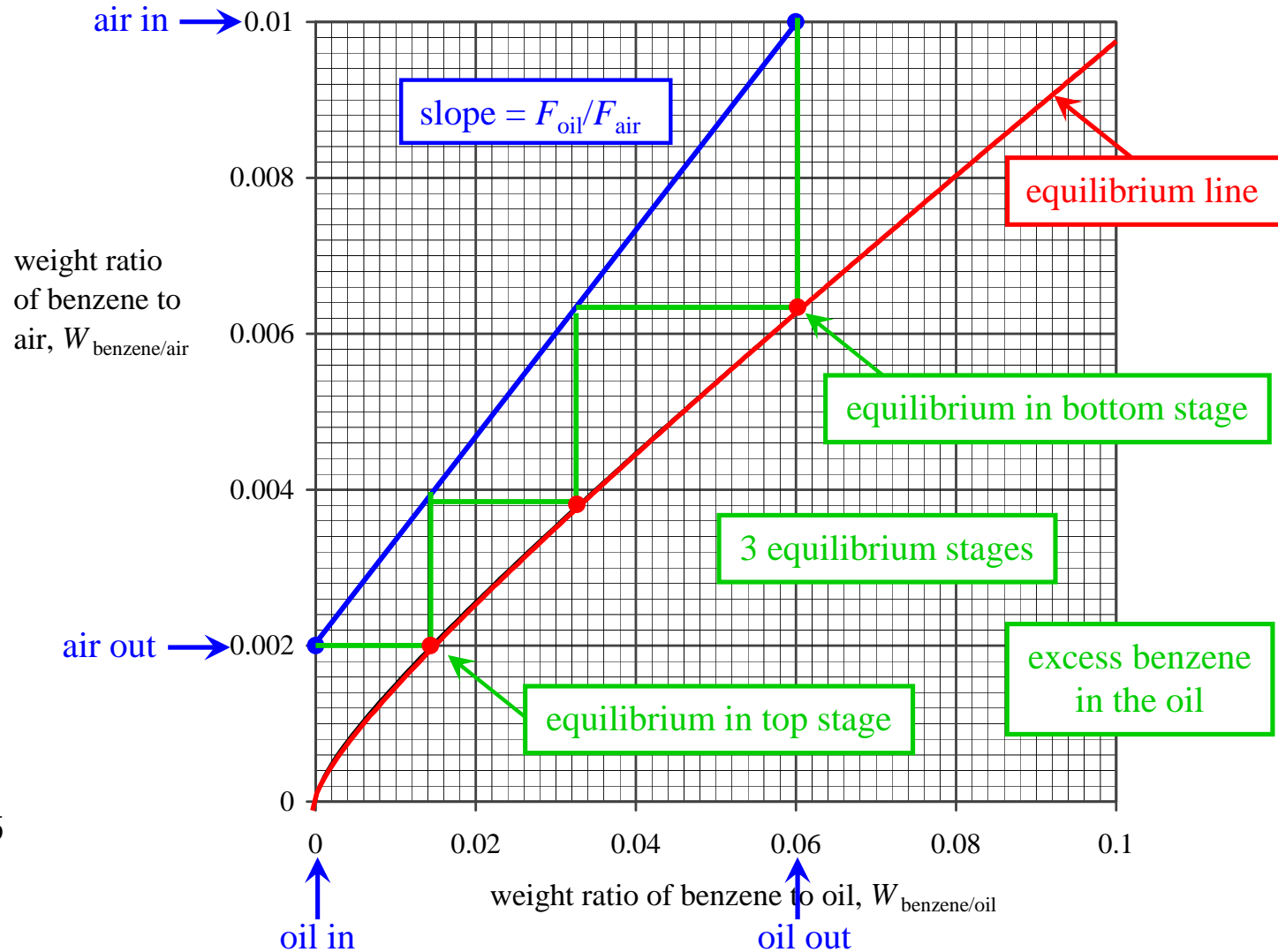
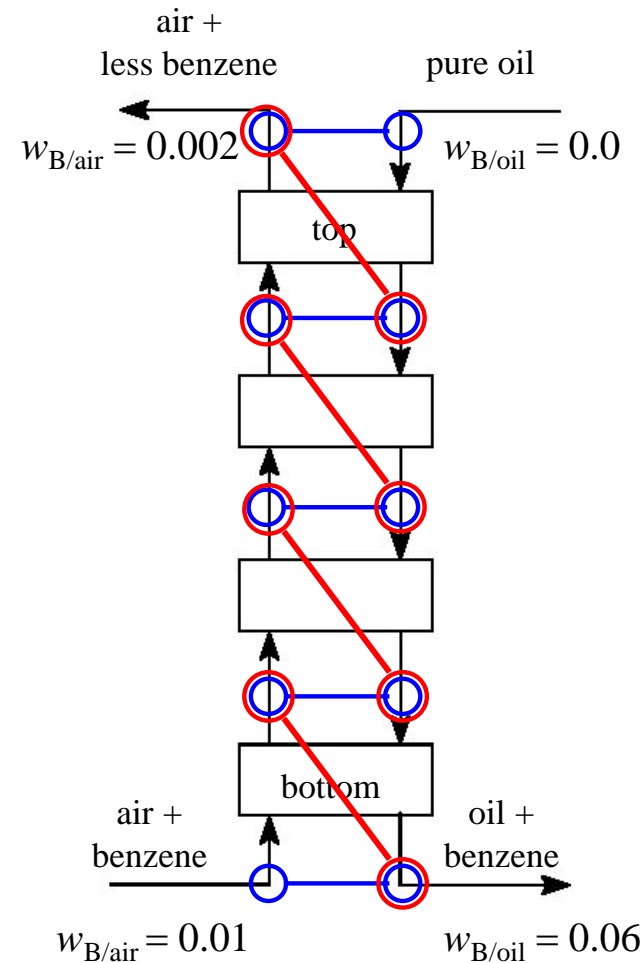
All (x,y) pairs leaving an equilibrium stage lie on the equilibrium line.

All adjacent (x,y) pairs lie on a line with slope  $F_{oil}/F_{air}$ .

This line is the *Operating Line*.

# Graphical Analysis of Multi-Stage Counter-Current Absorbers: Example 1

All compositions given. Calculate  $F_{\text{oil}}/F_{\text{air}}$  and number of stages.



**All** adjacent  $(x, y)$  pairs lie on a line with slope  $F_{\text{oil}}/F_{\text{air}}$ .

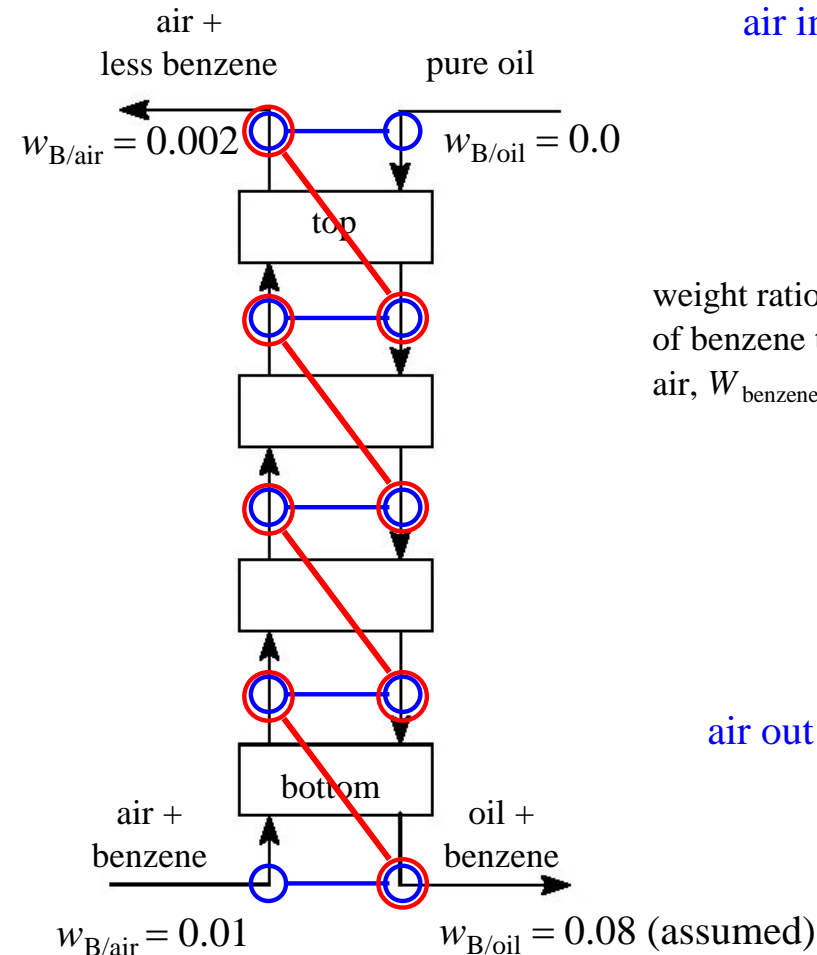
This line is the **Operating Line**.

**All**  $(x, y)$  pairs leaving an equilibrium stage lie on the equilibrium line.

1. Plot  $(x, y)$  pairs corresponding to top and bottom of absorber column.
2. Draw Operating Line.
3. Step off equilibrium stages.

# Graphical Analysis of Multi-Stage Counter-Current Absorbers: Example 2

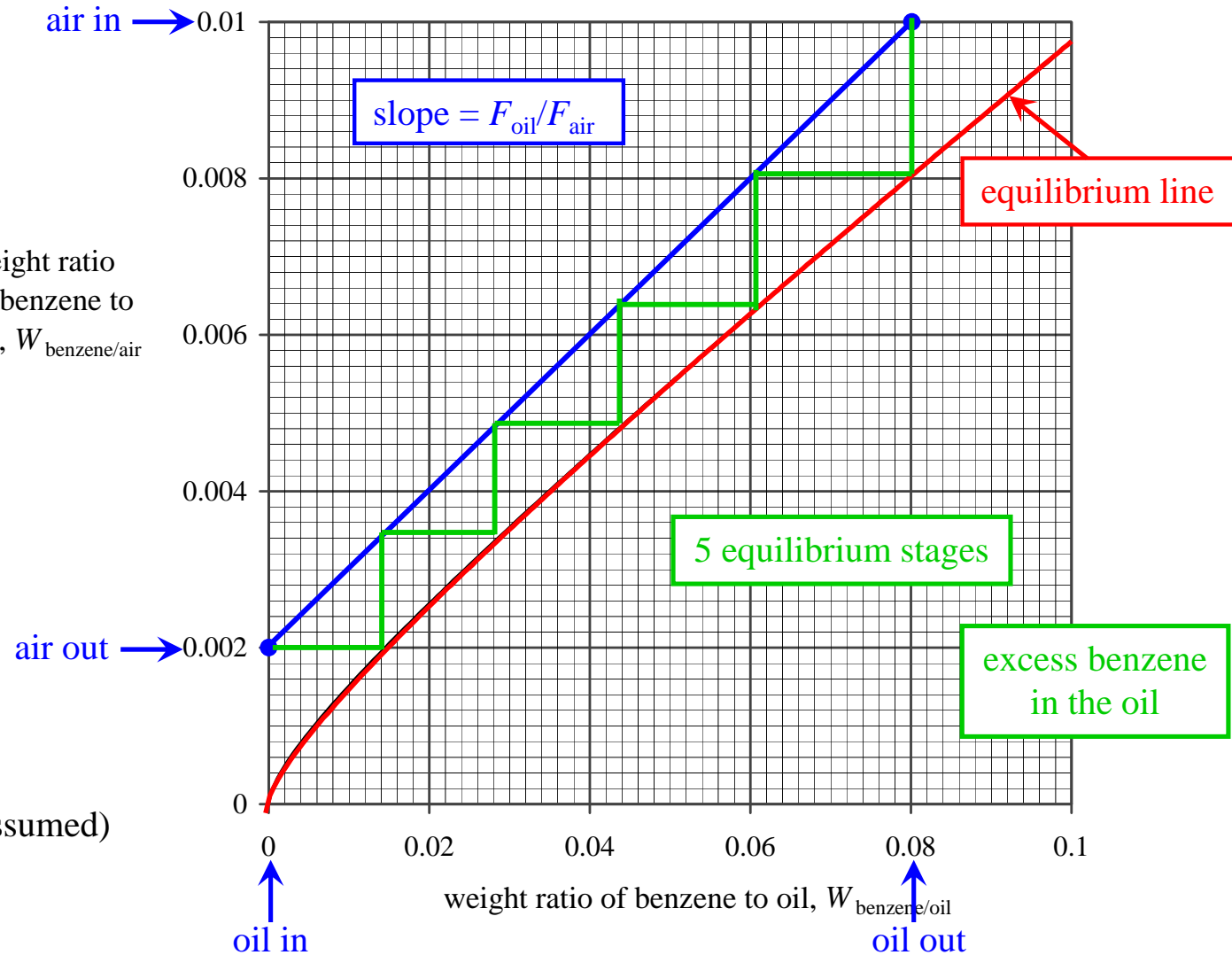
Decrease  $F_{oil}$  (and thus increase  $w_{B/oil,out}$ ).



**All** adjacent (x, y) pairs lie on a line with slope  $F_{oil}/F_{air}$ .

This line is the **Operating Line**.

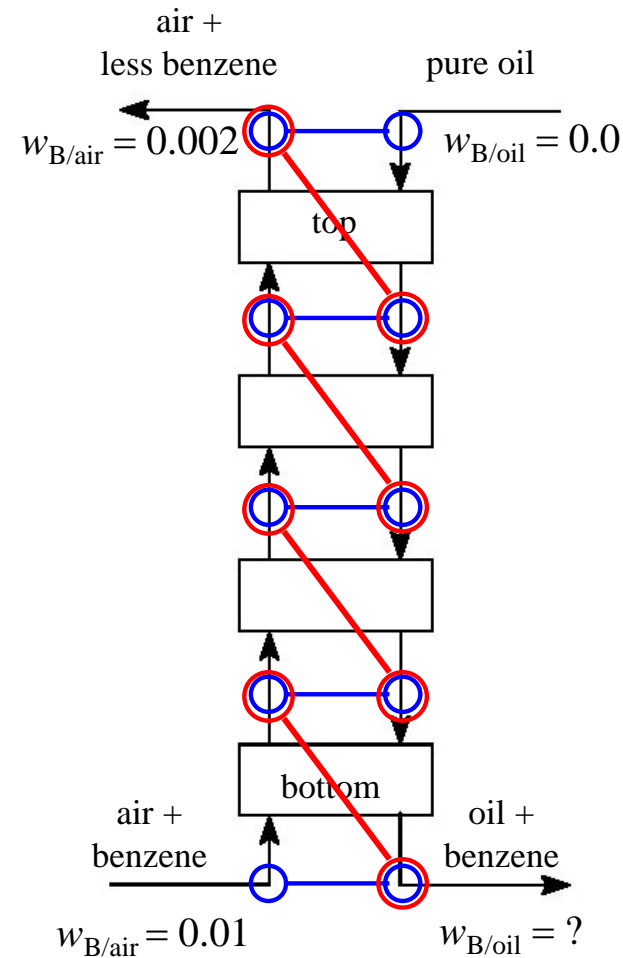
**All** (x,y) pairs leaving an equilibrium stage lie on the equilibrium line.



1. Plot (x, y) pairs corresponding to top and bottom of absorber column.
2. Draw Operating Line.
3. Step off equilibrium stages.

# Graphical Analysis of Multi-Stage Counter-Current Absorbers: Example 3

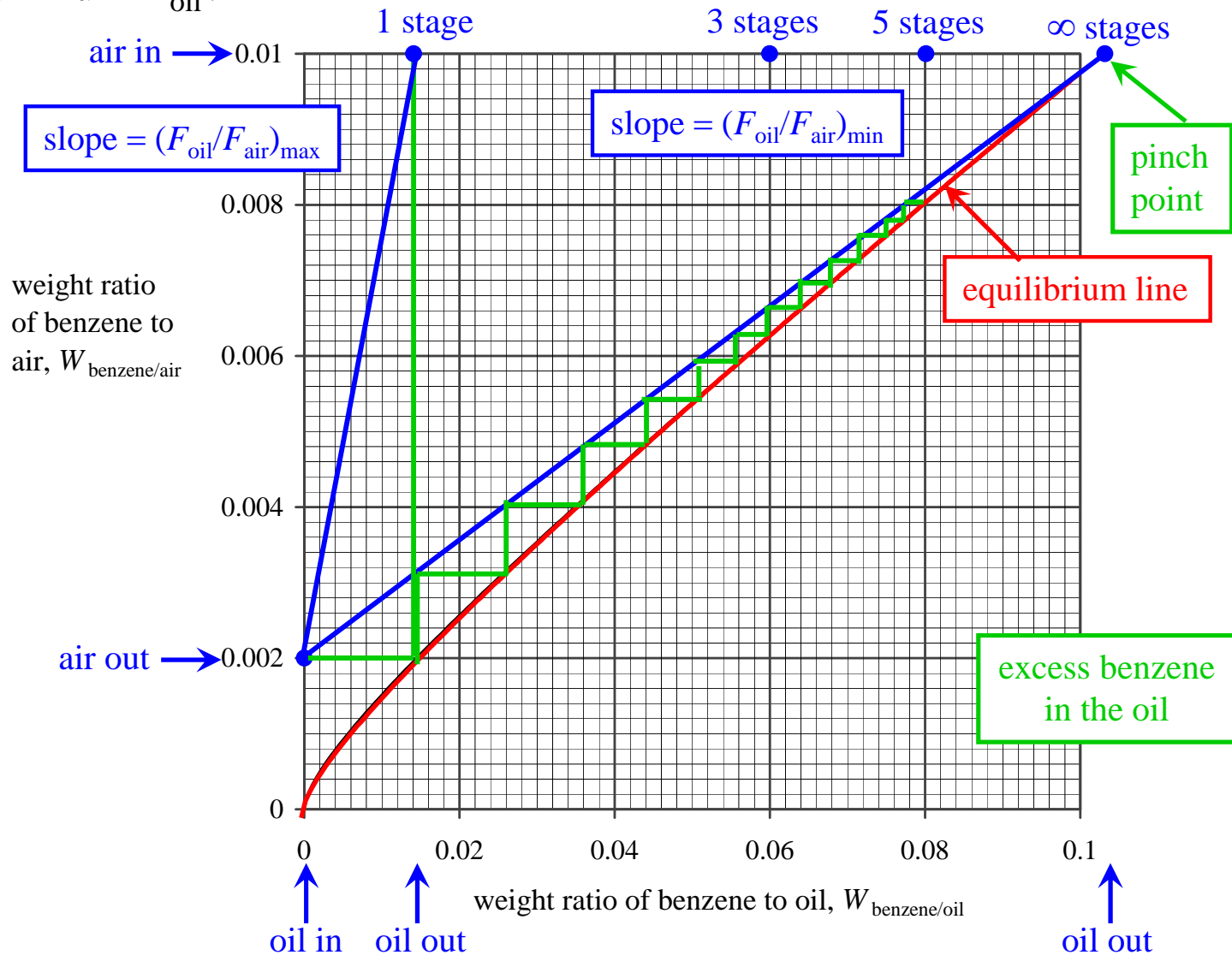
Minimum  $F_{oil}$ ? Maximum  $F_{oil}$ ?



*All* adjacent (x, y) pairs lie on a line with slope  $F_{oil}/F_{air}$ .

This line is the **Operating Line**.

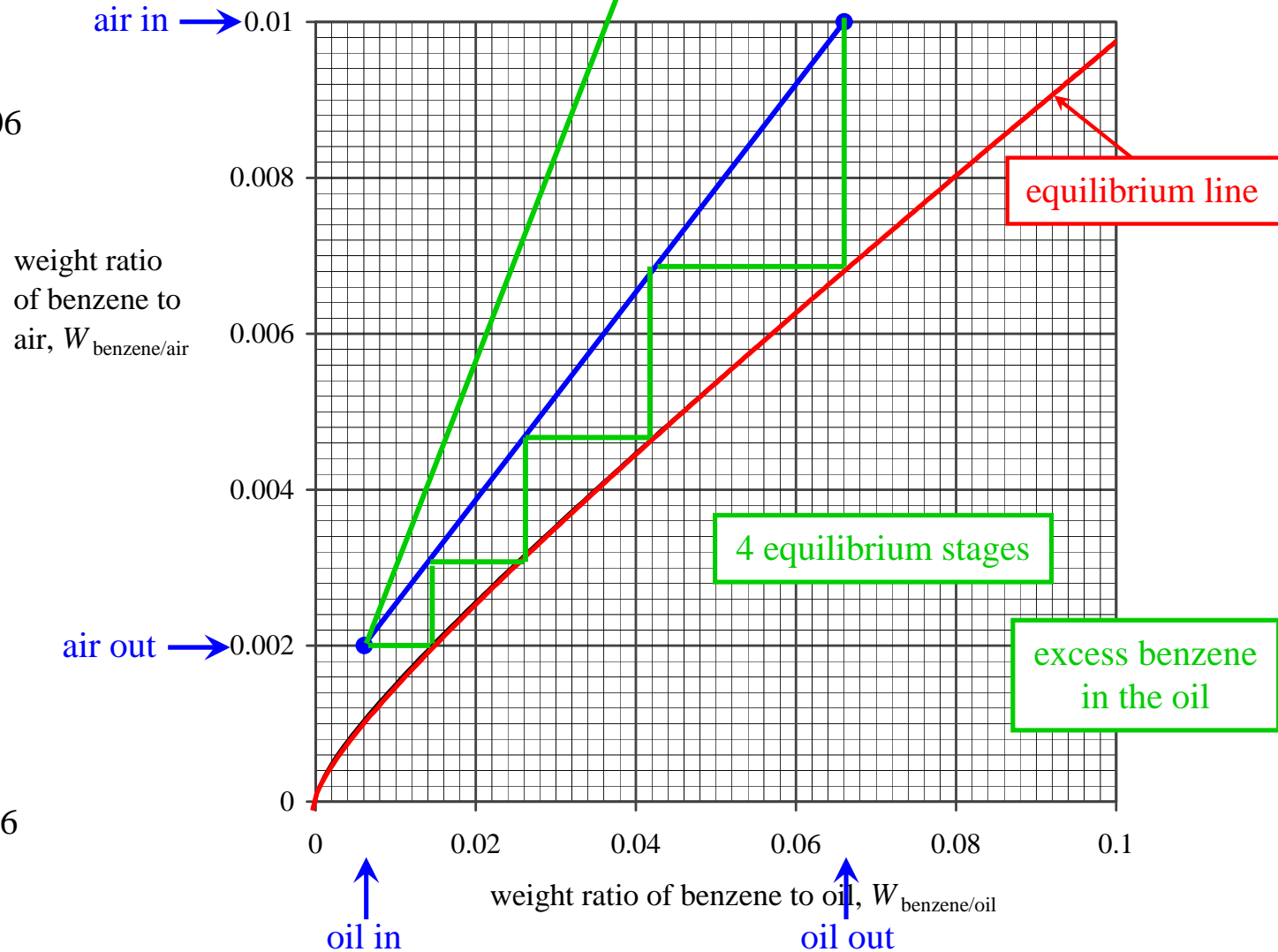
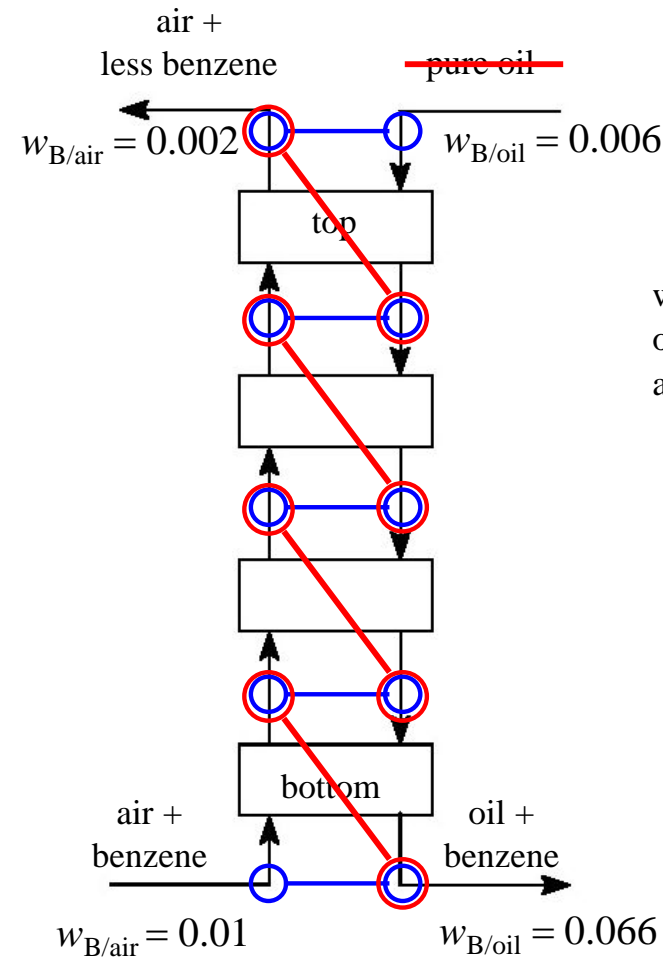
All (x,y) pairs leaving an equilibrium stage lie on the equilibrium line.





# Graphical Analysis of Multi-Stage Counter-Current Absorbers: Example 4 0.012

Oil feed contains benzene;  $F_{\text{oil}}/F_{\text{air}}$  same as example 1.



*All* adjacent  $(x, y)$  pairs lie on a line with slope  $F_{\text{oil}}/F_{\text{air}}$ .

This line is the **Operating Line**.

All  $(x, y)$  pairs leaving an equilibrium stage lie on the equilibrium line.

Example 5. Air in contains more benzene;  $w_{\text{B/air}} = 0.012$ .  
How to change operating line to reach  $w_{\text{B/air}} = 0.002$  in 4 stages?